

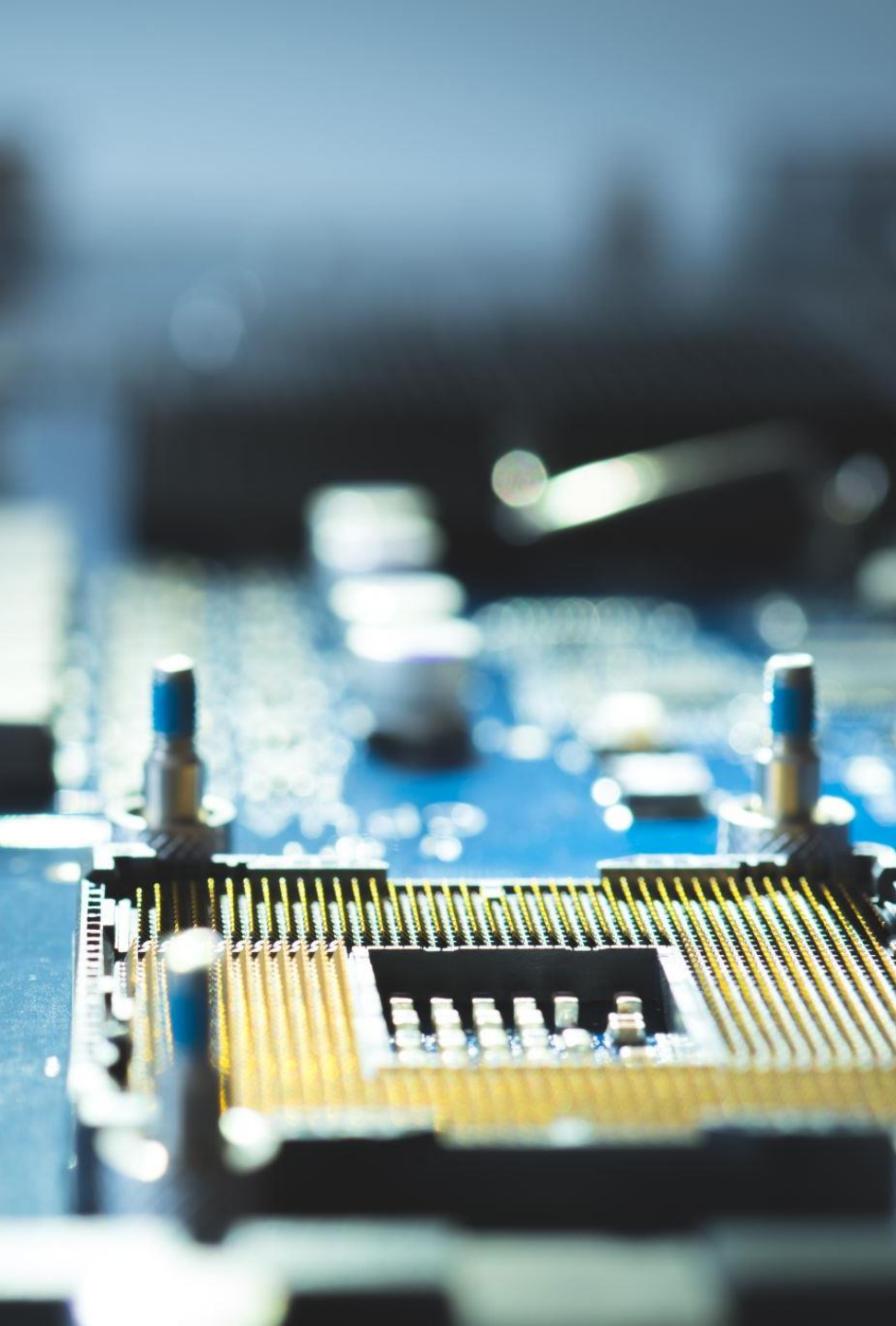
# MODELING IN MECHANICAL, ELECTRICAL, FLUID, AND THERMAL SYSTEMS – PART 3/3

(IN THE TIME DOMAIN)

POLYTECHNIC UNIVERSITY OF PR – ORLANDO CAMPUS

MECHANICAL ENGINEERING DEPARTMENT

PROF. EDUARDO VERAS, PHD.



# Learning Outcomes

---

- Describe the State-Space Model for Representing Physical Systems.
- Describe the State-Space Model for the Liquid-Level System - Example.
- Describe the State-Space Model for the Thermal System – Example.



Part #3:  
State-Space Model for Thermal Systems

# State-Space Model for the Thermal System

- Thermal systems are those that involve the transfer of heat from one substance to another.
- There are three different ways heat can flow from one substance to another: conduction, convection, and radiation. (Here we consider only conduction and convection).
- For conduction or convection heat transfer, the heat flow is:

$$q = K\Delta\theta$$

Eq. (3-18)

# State-Space Model for the Thermal System

Where:

$q$ := is the heat flow rate,  $kcal/sec$ ,

$\Delta\theta$ := is the temperature difference,  $^{\circ}C$ .

$K$ := is the coefficient,  $kcal/sec.^{\circ}C$ .

- *For conduction*, the coefficient  $K = \frac{kA}{\Delta X}$  where:

$k$ := is the thermal conductivity,  $kcal/m\ sec\ ^{\circ}C$

$A$ := is the area normal to heat flow,  $m^2$ .

$\Delta X$ := is the thickness of the conductor, m.

# State-Space Model for the Thermal System

- *For convection*, the coefficient  $K = HA$  where:

$H$ := is the convection coefficient,  $\frac{kcal}{m^2 \text{ sec } ^\circ\text{C}}$

$A$ := is the area normal to heat flow,  $m^2$ .

- The thermal resistance  $R$  for heat transfer between two substances may be defined as follows:

$$R = \frac{\text{change in the temperature difference, } ^\circ\text{C}}{\text{change in the heat flow rate, } \frac{kcal}{^\circ\text{C}}} \quad \text{Eq. (3-19)}$$

# State-Space Model for the Thermal System

- The thermal resistance for conduction or convection heat transfer is given by:

$$R = \frac{d(\Delta\theta)}{dq} = \frac{1}{K} \quad \text{Eq. (3-20)}$$

- Since the thermal conductivity and convection coefficients are almost constant, the thermal resistance for either conduction or convection is constant.

# State-Space Model for the Thermal System

- The thermal capacitance  $C$  is defined by:

$$C = \frac{\text{change in heat stored, kcal}}{\text{change in temperature, } ^\circ\text{C}} \quad \text{Eq. (3-21)}$$

Or:

$$C = mc \quad \text{Eq. (3-22)}$$

Where:

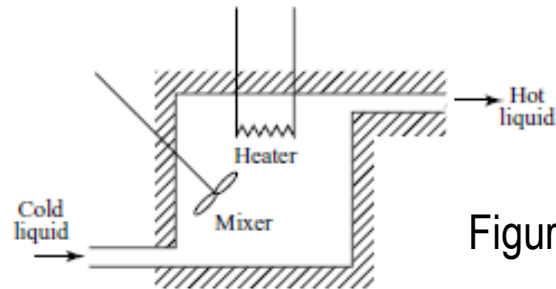
$m$  := mass of substance considered,  $kg$

$c$  := specific heat of substance,  $\frac{kcal}{kg \text{ } ^\circ\text{C}}$



# State-Space Model for the Thermal System

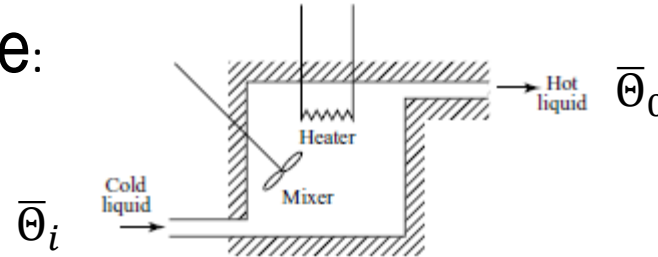
- Consider the system shown in Figure 3-3:



- Assumptions made:
  - tank is insulated to eliminate heat loss to the surrounding air.
  - there is no heat storage in the insulation
  - the liquid in the tank is perfectly mixed so that it is at a uniform temperature.
- *Therefore, a single temperature is used to describe the temperature of the liquid in the tank and of the outflowing liquid.*

# State-Space Model for the Thermal System

- In Figure 3-3, the variables are:



$\bar{\Theta}_i$  := steady-state temperature of inflowing liquid, °C

$\bar{\Theta}_0$  := steady-state temperature of outflowing liquid, °C

$G$  := steady-state liquid flow rate,  $kg/sec$

$M$  := mass of liquid in the tank,  $kg$

$c$  := specific heat of liquid,  $kcal/kg\ ^\circ C$

$R$  := thermal resistance,  $^\circ C sec/kcal$

$C$  := thermal capacitance,  $kcal/^\circ C$

$\bar{H}$  := steady-state heat input rate,  $kcal/sec$

# State-Space Model for the Thermal System

- We can obtain the dynamic equation given the following conditions:
  1. The temperature of the inflowing liquid is suddenly changed from  $\bar{\Theta}_i$  to  $\bar{\Theta}_i + \theta_i$  while the heat input rate  $H$ .
  2. The liquid flow rate  $G$  are kept constant.
  3. The heat outflow rate is changed from  $\bar{H}$  to  $\bar{H} + h_0$ .
  4. The temperature of the outflowing liquid will be changed from  $\bar{\Theta}_0$  to  $\bar{\Theta}_0 + \theta_0$ .
- For these conditions, the *heat balance equation* for this case is:  $C \frac{d\theta}{dt} = Gc\theta_i - h_0$  Eq. (3-23)
- Substituting Eq. (3-20) into Eq. (3-23), yields:  $RC \frac{d\theta}{dt} + \theta = \theta_i$  Eq. (3-24)

# State-Space Model for the Thermal System: An Example

- Now, we derive the *state-space model for thermal control* system considering small deviations from steady-state operation. Assume that the heat loss to the surroundings is negligible.

- **Solution:**

- From Eq. (3-24):  $RC \frac{d\theta}{dt} + \theta = \theta_i$

- From Eq. (3-20):  $Rdq = d\theta$

- The heat transfer results in a change in the system's temperature. So, taking the heat flow and temperature changes over a time interval,  $dt$ , Eq. (3-20) becomes:

$$R \frac{dq}{dt} = \frac{d\theta}{dt}$$

# State-Space Model for the Thermal System: An Example

- Solution (cont.): Changing notation:

$$RC \frac{d\theta}{dt} + \theta(t) = \theta_i(t) \quad \rightarrow \quad RC\dot{\theta}(t) + \theta(t) = \theta_i(t) \quad \text{(a)}$$

$$R \frac{dq}{dt} = \frac{d\theta}{dt} \quad \rightarrow \quad Rq\dot{(t)} = \dot{\theta}(t) \quad \text{(b)}$$

- From Eq. (a): 
$$\dot{\theta}(t) = -\frac{1}{RC}\theta(t) + \frac{1}{RC}\theta_i(t) \quad \text{(c)}$$

- **Note:** Recall that  $C = \frac{dq}{d\theta}$  and deriving  $q = mc\theta$ , we get  $dq = mcd\theta$  (or  $\frac{dq}{d\theta} = mc$ ), where  $c$  is the specific heat of the liquid and  $m$  is the mass of liquid in the tank. Then:

$$C = mc \quad \text{(d)}$$

$$q = C\theta \quad \text{(e)}$$

# State-Space Model for the Thermal System: An Example

- Solution (cont.): Substituting Eq (b) and Eq. (e) into Eq. (c), we get:

$$R\dot{q}(t) = \dot{\theta}(t) \quad q(t) = C\theta(t) \quad \dot{\theta}(t) = -\frac{1}{RC}\theta(t) + \frac{1}{RC}\theta_i(t)$$

$$\rightarrow R\dot{q}(t) = -\left(\frac{1}{RC}\right)\left(\frac{1}{C}\right)q(t) + \frac{1}{RC}\theta_i(t) \quad \therefore \dot{q}(t) = -\frac{1}{R^2C^2}q(t) + \frac{1}{R^2C}\theta_i(t) \quad \text{(f)}$$

- Let us define state variables  $x_1(t)$  and  $x_2(t)$  as:

$$x_1(t) = \theta(t) \quad \text{(g)}$$

$$x_2(t) = q(t) \quad \text{(h)}$$

# State-Space Model for the Thermal System: An Example

- Solution (cont.):

- From Eq. (g):  $\dot{x}_1(t) = \dot{\theta}(t) \Rightarrow \dot{x}_1(t) = \dot{\theta}(t) = -\frac{1}{RC}\theta(t) + \frac{1}{RC}\theta_i(t)$  Eq. (i)

- From Eq. (h):  $\dot{x}_2(t) = \dot{q}(t) \Rightarrow \dot{x}_2(t) = \dot{q}(t) = -\frac{1}{R^2C^2}q(t) + \frac{1}{R^2C}\theta_i(t)$  Eq. (j)

- Dropping  $t$  from Eq. (i) & Eq. (h), the state-space model in matrix form is:  $\dot{x}(t) = Ax(t) + Bu(t)$

State Equation: 
$$\begin{bmatrix} \dot{x}_1 \\ \dot{x}_2 \end{bmatrix} = \begin{bmatrix} -\frac{1}{RC} & 0 \\ 0 & -\frac{1}{(RC)^2} \end{bmatrix} \begin{bmatrix} x_1 \\ x_2 \end{bmatrix} + \begin{bmatrix} \frac{1}{RC} \\ \frac{1}{R^2C} \end{bmatrix} u$$

Output Equation: 
$$y = [1 \quad 1] \begin{bmatrix} x_1 \\ x_2 \end{bmatrix}$$

$$y(t) = Cx(t) + Du(t)$$

# State-Space Model for Representing Physical Systems

- In the state-space model representation, the numbers of **state variables** is equal with the **highest-order of the ordinary differential equation (ODE)** describing the dynamic system.
- The set of **state variables** is not unique, and they may be defined in terms of physical variables which can be measured.
- *State-space models* are the cornerstone of modern control theory.





POLYTECHNIC UNIVERSITY OF PR – ORLANDO CAMPUS. MECHANICAL ENGINEERING DEPARTMENT. PROF. EDUARDO VERAS, PHD.

# THANK YOU

POLYTECHNIC UNIVERSITY OF PR  
– ORLANDO CAMPUS

MECHANICAL ENGINEERING  
DEPARTMENT

PROF. EDUARDO VERAS, PHD.

[EVERAS@PUPR.EDU](mailto:EVERAS@PUPR.EDU)